Amendments to the Specification:

Please replace paragraph [0021] with the following amended paragraph:

[0020] In a preferred configuration, the evaporation unit comprises a

plurality of channels as shown in Figure 3 which are arranged parallel to one

another, since it is expedient to supply a plurality of smaller channels of the

evaporation unit with heat than to supply a large central evaporation unit. The

surface area of the evaporation unit is increased, which leads to improved heat

transfer between catalyst layer and evaporation unit. The branching also

readily allows multiple contact with the catalyst layers, for example by an

arrangement in which one or more bores are guided onto each catalyst layer, and

the evaporation unit is then arranged in these bores. However, this too is

dependent on the reactor design and the reaction which is to be carried out.

Please replace paragraph [0034] with the following amended paragraph:

[0034] An evaporation unit 2 in which a liquid starting material 1 is

evaporated adjoins the chambers 9, 10, 11. The starting material is fed to the

chambers 9, 10, 11 as starting-material vapor 3 via outlet means 5, 6, 7 of a

distributor system 4. The evaporation unit 2 is in substantially direct contact

with the hot reactor zone, preferably in direct contact with the hot catalyst layers

of the chambers 9, 10, 11 (i.e., the area of the evaporation unit 2 in which the

evaporation substantially takes place is at least partially surrounded by the

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chambers 9, 10, 11 and therefore by the hot reactor zone). The evaporation unit

2 may be arranged in such a way that it is completely surrounded by the

chambers (as shown in Figure 2), or it may be arranged on the edge region, in

such a way that it is at least partially surrounded by the chambers 9, 10, 11 (e.g.,

that it laterally adjoins these chambers, as illustrated in Fig. 1). In this case, the

evaporation area is in each case arranged at the level of the hot reactor zone of

the chambers 9, 10, 11, substantially parallel thereto.

Please replace paragraph [0037] with the following amended paragraph:

[0037] Preferably in each case one outlet 5, 6, 7 is assigned to each

catalyst-containing chamber 9, 10, 11, in order to distribute the starting-material

vapor 3 as uniformly as possible. In a preferred embodiment, one outlet 5, 6, 7

projects into the associated chamber 9, 10, 11. The starting material 3 in vapor

form is admitted to the corresponding chambers 9, 10, 11 and is reacted in the

chambers 9, 10, 11. The reaction generates heat, which in turn is made available

for evaporation of the liquid starting material 1 in the evaporation unit 2. The

device according to the present invention also has means 8, 12 which are known

per se for discharging the products, the reacted products of the starting material

3 being passed out of discharge means 8 into a collection manifold 12. This

configuration can be used to provide hydrogen to a fuel cell of a fuel cell system

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Please add the following new paragraph after paragraph [0046]:

[0046.1] In a preferred configuration, the evaporation unit comprises a

plurality of channels as shown in Figure 3 which are arranged parallel to one

another, since it is expedient to supply a plurality of smaller channels of the

evaporation unit with heat than to supply a large central evaporation unit. The

surface area of the evaporation unit is increased, which leads to improved heat

transfer between catalyst layer and evaporation unit. The branching also

readily allows multiple contact with the catalyst layers, for example by an

arrangement in which one or more bores are guided onto each catalyst layer, and

the evaporation unit is then arranged in these bores. However, this too is

dependent on the reactor design and the reaction which is to be carried out.